

PIR for Hydrogen and Carbon Dioxide Pipelines

Some Thoughts on Hazard Modelling

presented by
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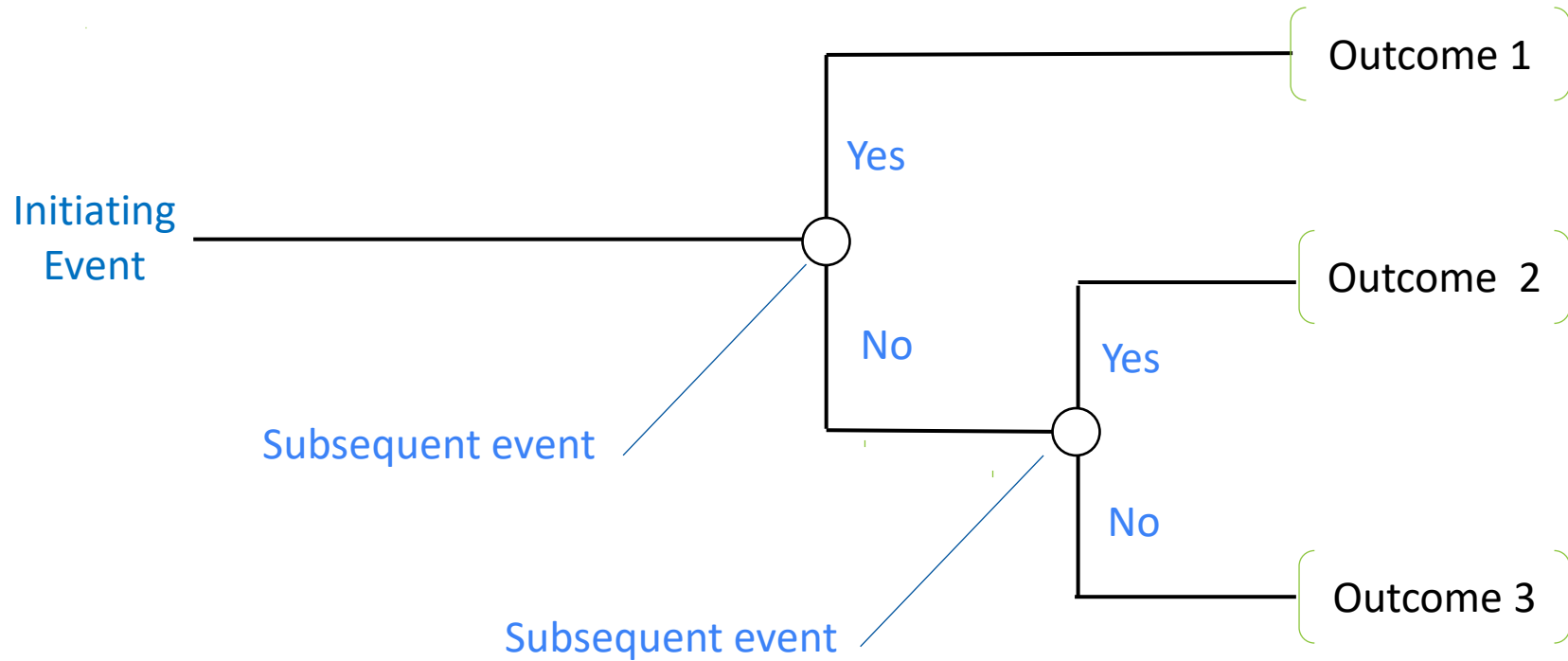
PHMSA Public Meeting, Houston, TX
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Product Characteristics

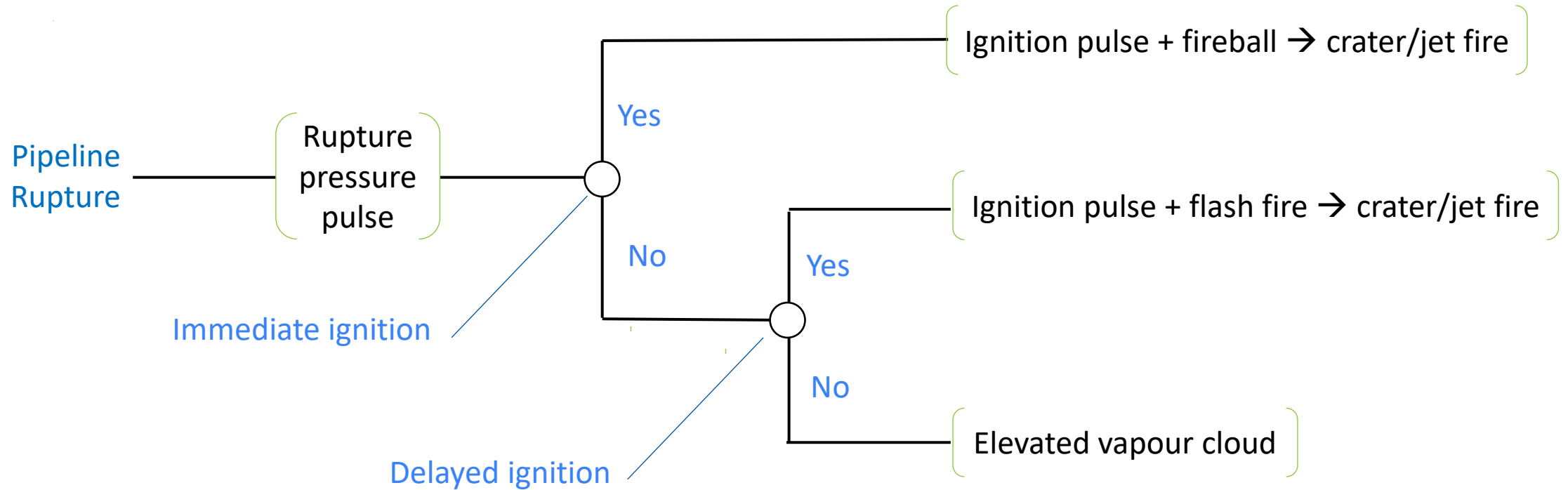
Attribute	Natural Gas	Hydrogen	Carbon Dioxide
Density (behaviour)	lighter than air (buoyant rise)	lighter than air (buoyant rise)	heavier than air (ground hugging)
Hazards	fires & explosions	fires & explosions	toxic & asphyxiating vapour
Concentration of interest	5 to 15% (flammable range)	4 to 75% (flammable range)	> about 60% (asphyxiation) > about 7% (toxicity)?
Fuel gas category	low reactivity	high reactivity	not applicable
Energy to ignite	high	low	not applicable
Flame speed	low	high	not applicable

Event Tree for Pipelines Transporting Buoyant Flammable Gases

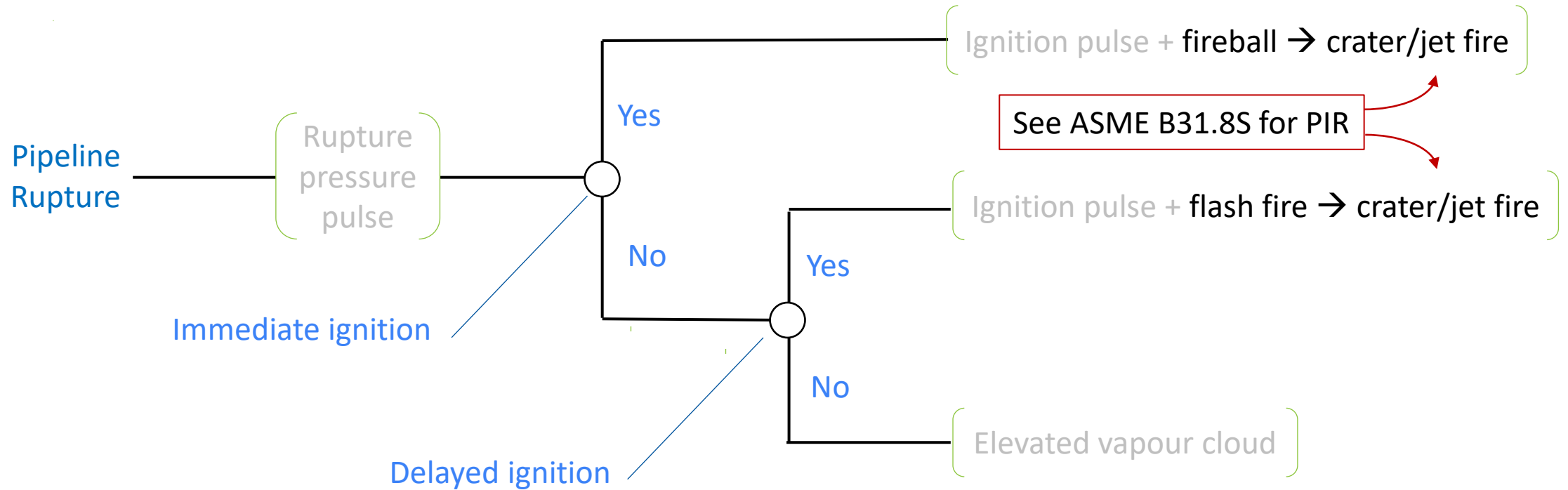
- What is an event tree?



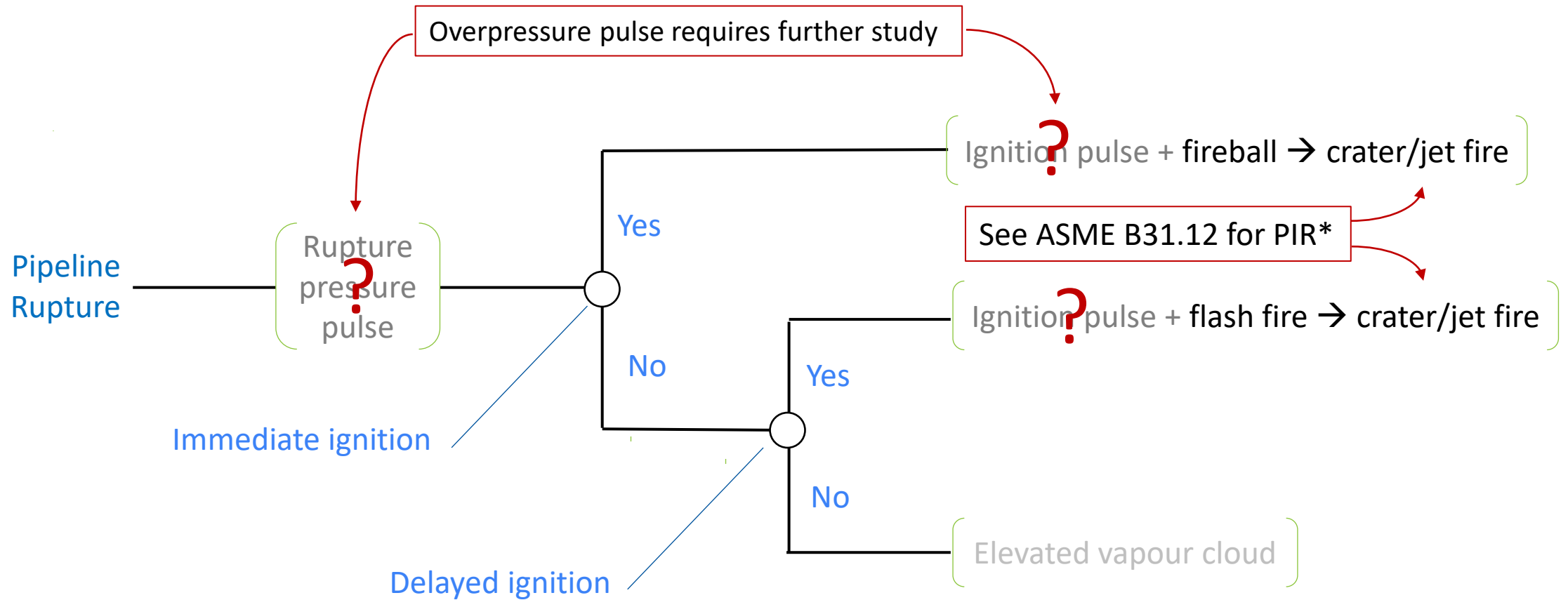
Event Tree for Pipelines Transporting Buoyant Flammable Gases



Event Tree for Pipelines Transporting Natural Gas

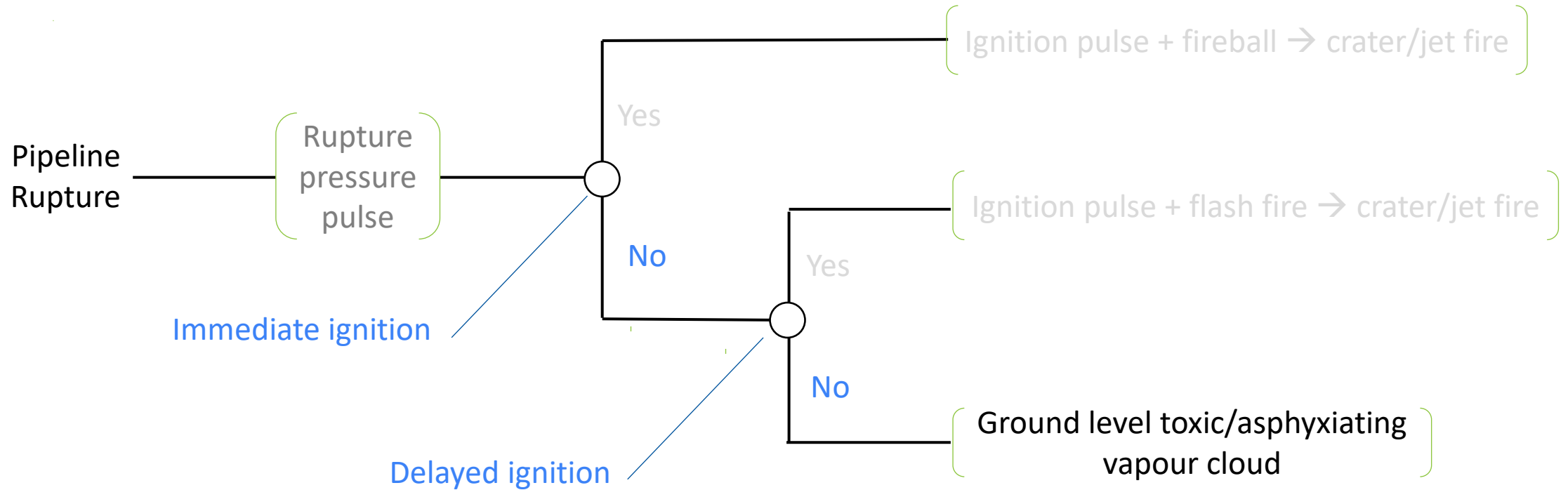


Event Tree for Pipelines Transporting Hydrogen Gas



**From 2005 PHMSA Report TT013 by Baker & C-FER
- based on outdated flame emissivity data
- requires updating*

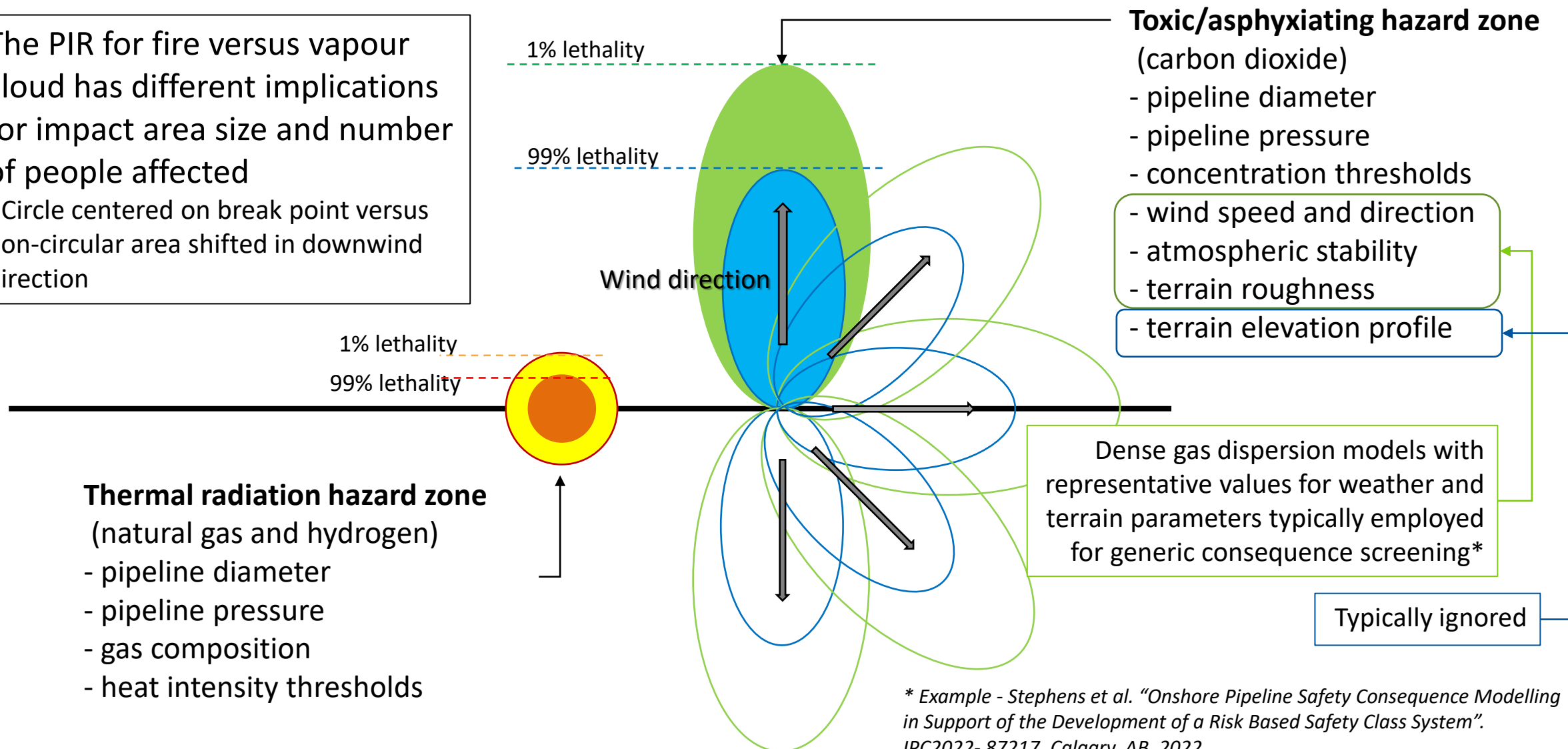
Event Tree for Pipelines Transporting Carbon Dioxide



Factors Affecting Potential Impact Areas

The PIR for fire versus vapour cloud has different implications for impact area size and number of people affected

- Circle centered on break point versus non-circular area shifted in downwind direction



* Example - Stephens et al. "Onshore Pipeline Safety Consequence Modelling in Support of the Development of a Risk Based Safety Class System". IPC2022- 87217. Calgary, AB, 2022.