

# Failure Investigation Forum

Partners In Pipeline Safety

December 13, 2022



U.S. Department of Transportation  
Pipeline and Hazardous Materials  
Safety Administration

Investigate - Analyze - Prevent

**PHMSA: Your Safety is Our Mission**



# Speakers

- Accident Trends and Recent Lessons Learned  
Brian Pierzina, PHMSA AID Accident Investigator
- NAPSIR Overview  
Jon Wolfgram, NAPSIR Chair
- Pipeline Safety Trust Update  
Bill Caram, Executive Director
- NTSB Update  
Sara Lyons, NTSB Accident Investigator
- Enforcement of Incidents and Accidents  
Rob Burrough, PHMSA Eastern Region Director



# Accident Trends and Lessons Learned

Accident Investigation Division  
December 13, 2022



# Discussion Topics

- Cause and Risk Factor Analysis – HELP TARGET RESOURCES
- Control Room Issues – THINK LEAK FIRST
- Integrity Assessment Concerns – ADD CONSERVATISM
- Excavation Damages – UNIQUE ISSUES WITH HDD



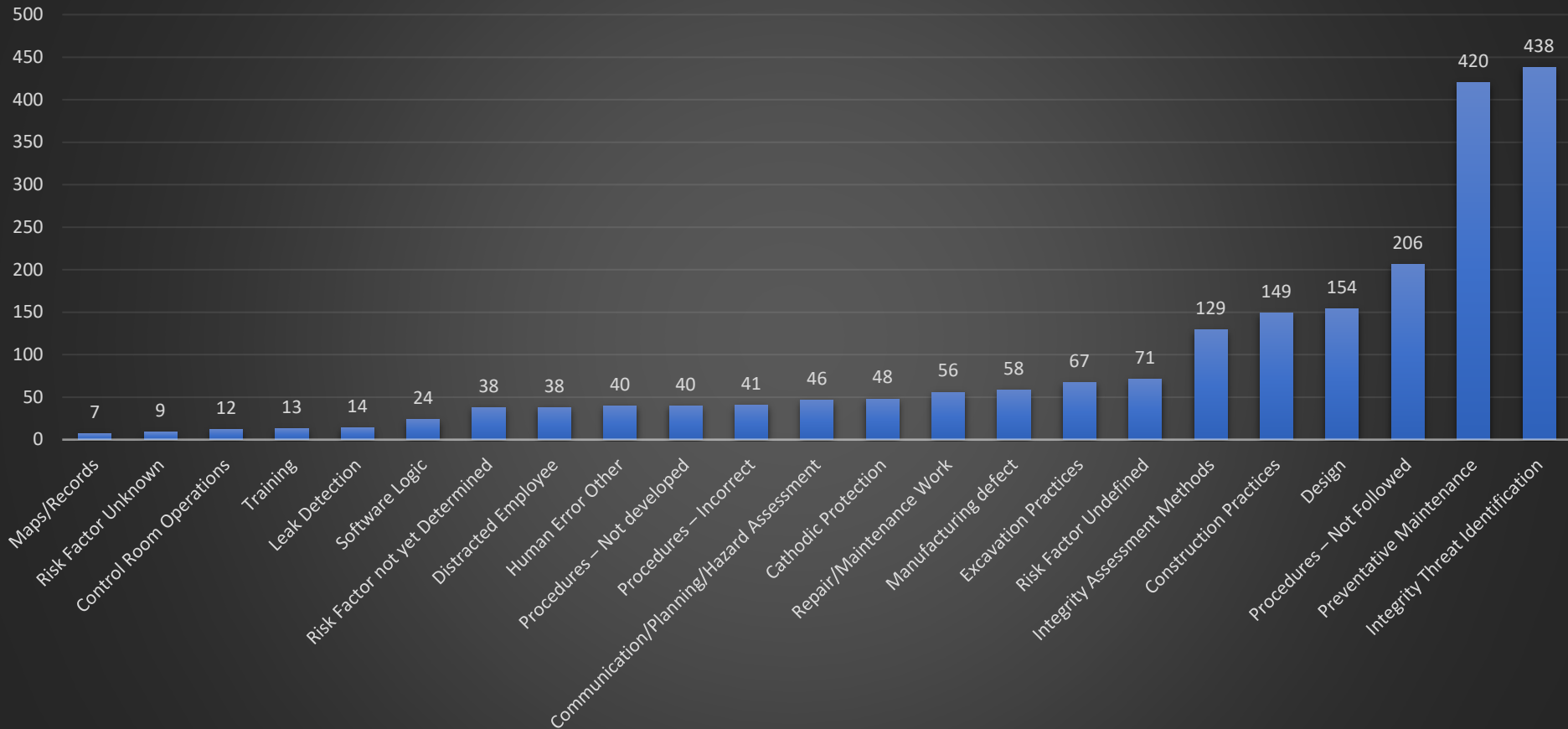
# Risk Factors

Cathodic Protection	Communication/Hazard Assessment
Construction	Control Room
Design	Distracted Employee
Human Error	Integrity Assessment Methods
Integrity Threat Identification	Leak Detection
Manufacturing Defect	Maps/Records
Preventative Maintenance	Training
Repair/Maintenance Work	Software Logic
Procedures – Incorrect, Not Developed, or Not Followed	Risk Factor – Undefined, Unknown, or Not Yet Determined



# All Risk Factors – All Products

## Failures 2018 - Present



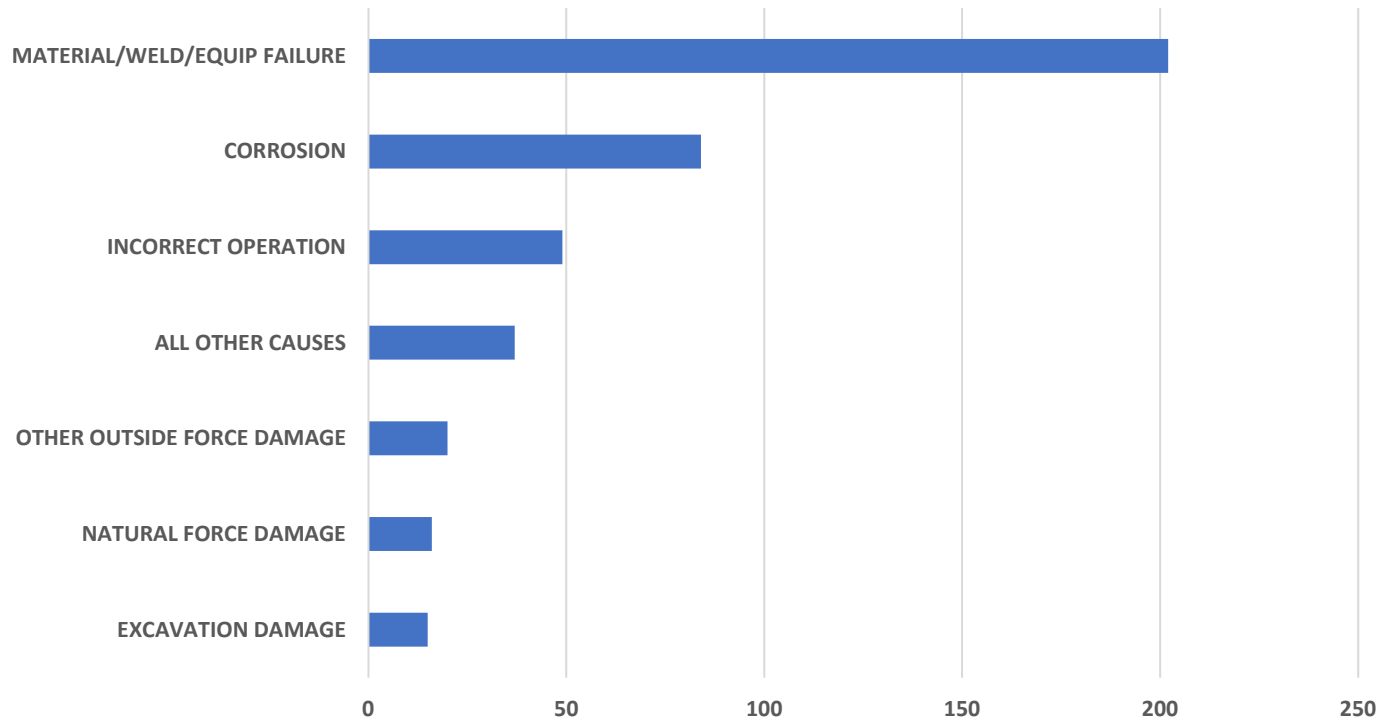
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# 30-Day Report Cause

Cause Type: Hazardous Liquid and Gas Transmission  
# Of Failures Last 12 Months



# Drilling into the Risk Factors

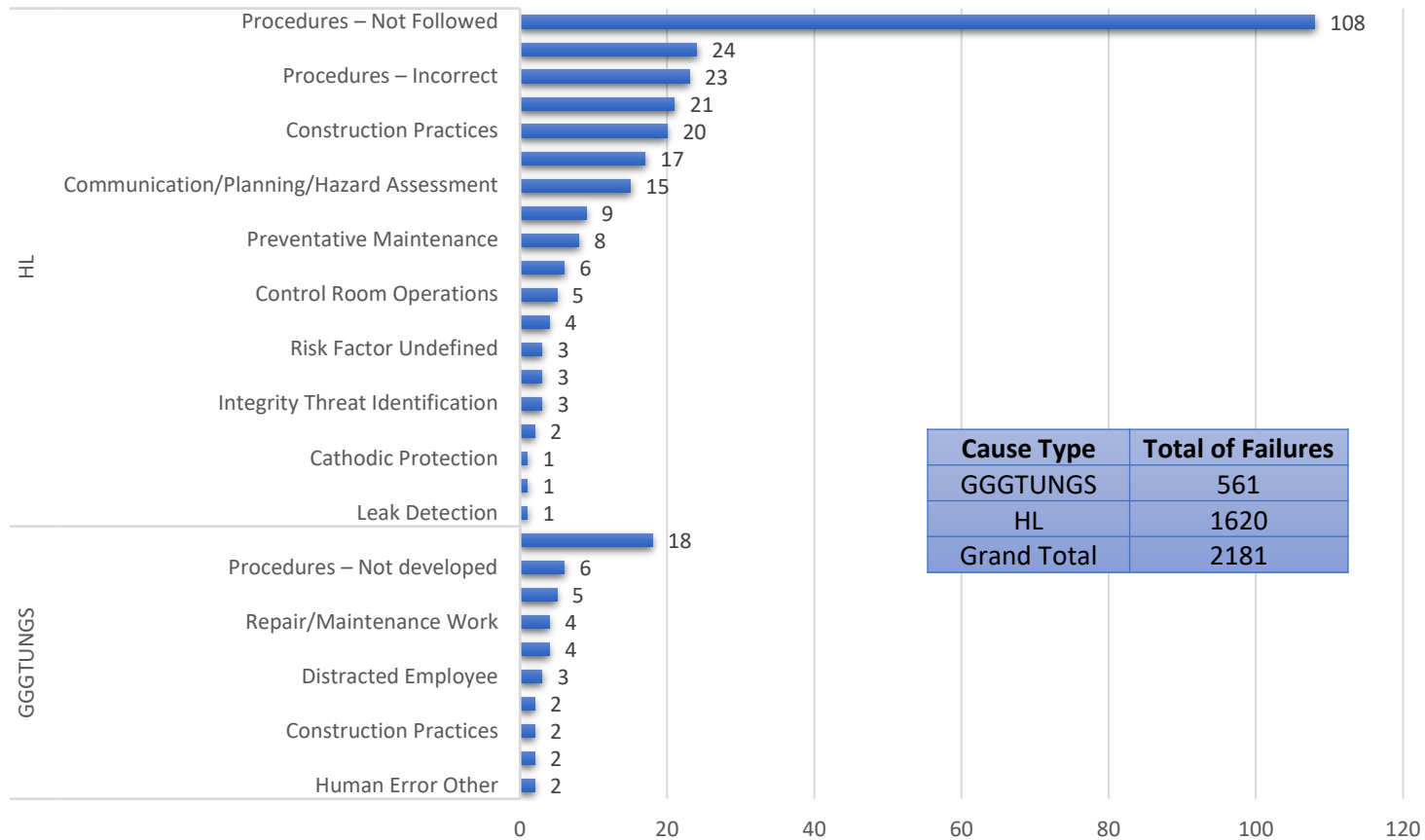
While covering these please consider the following:

- How can we identify these Risks?
- Does the code address them adequately?
- Do established processes help identify these issues?
- Does your training teach employees to look for these?





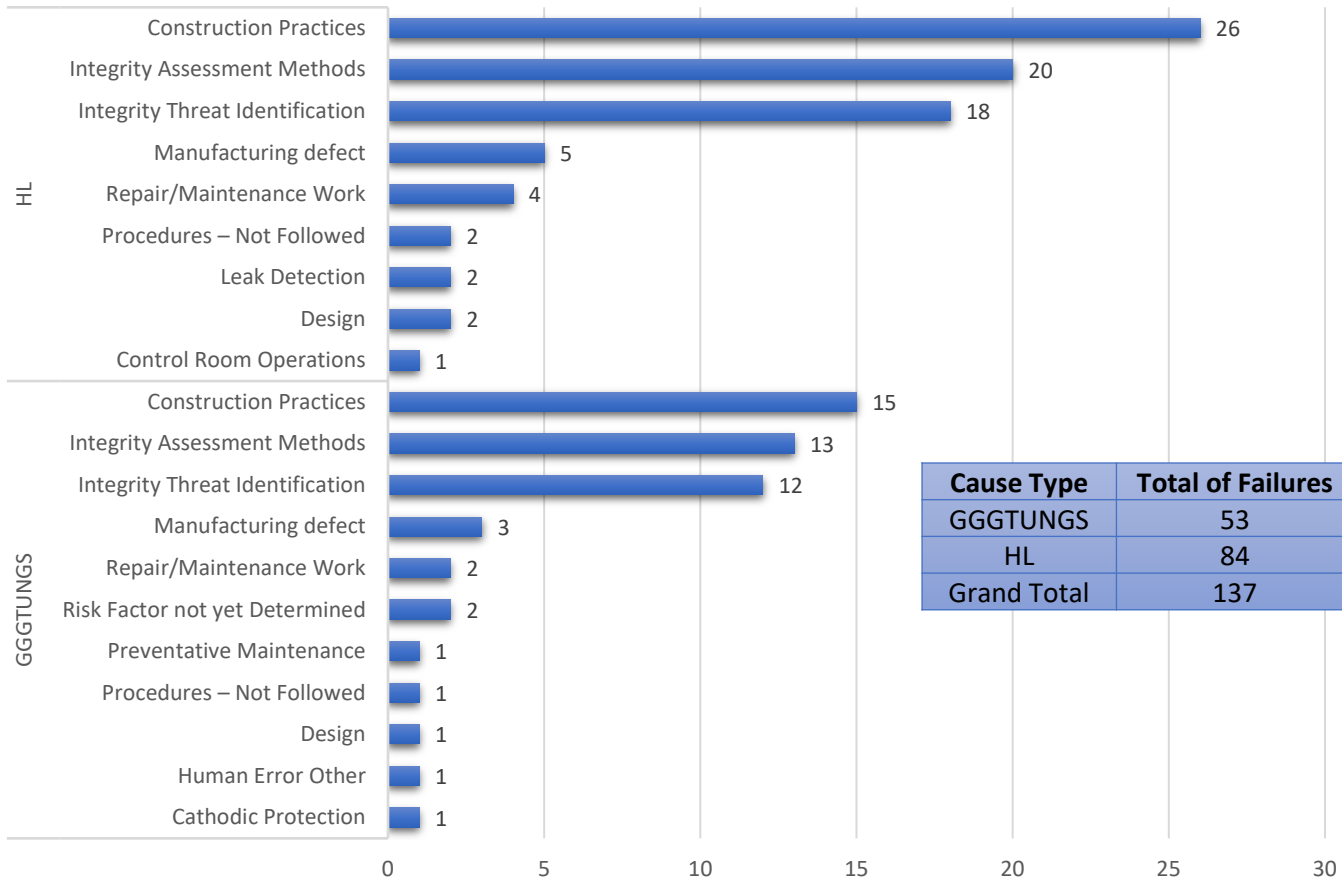
# Incorrect Operations – Risk Factors



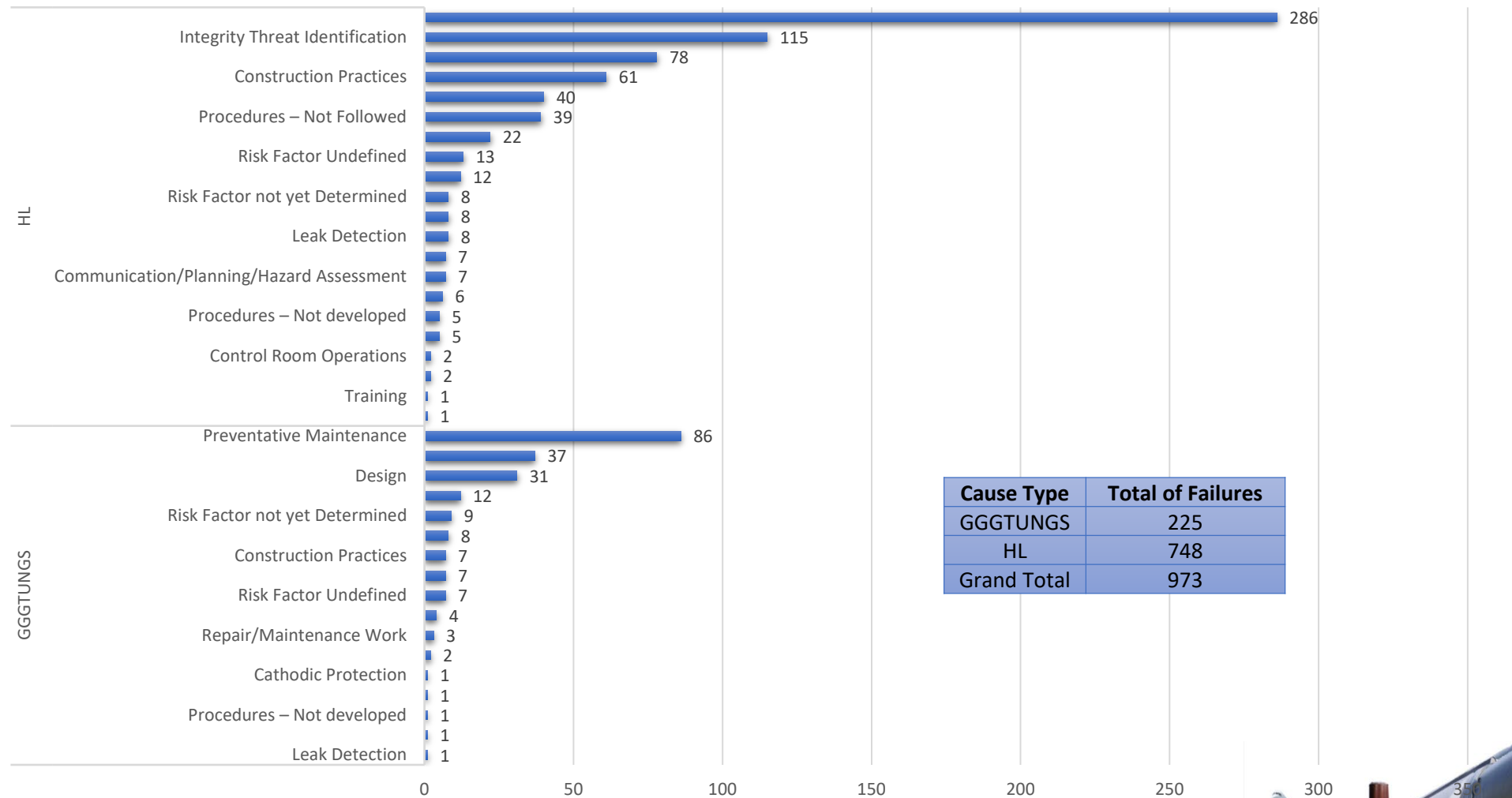
Cause Type	Total of Failures
GGGTUNGS	561
HL	1620
Grand Total	2181



# Material Failure – Risk Factors



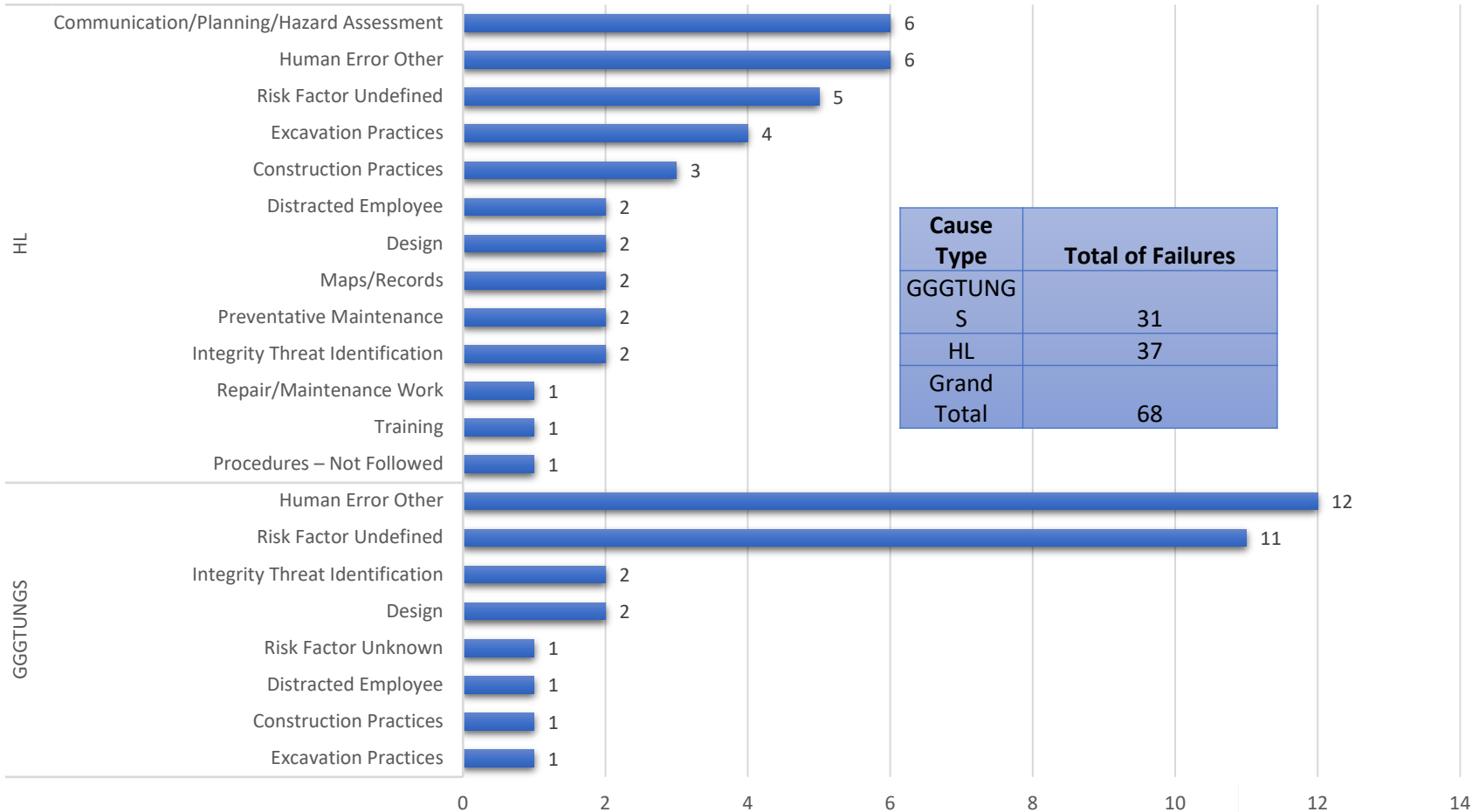
# Equipment Failure Risk Factors



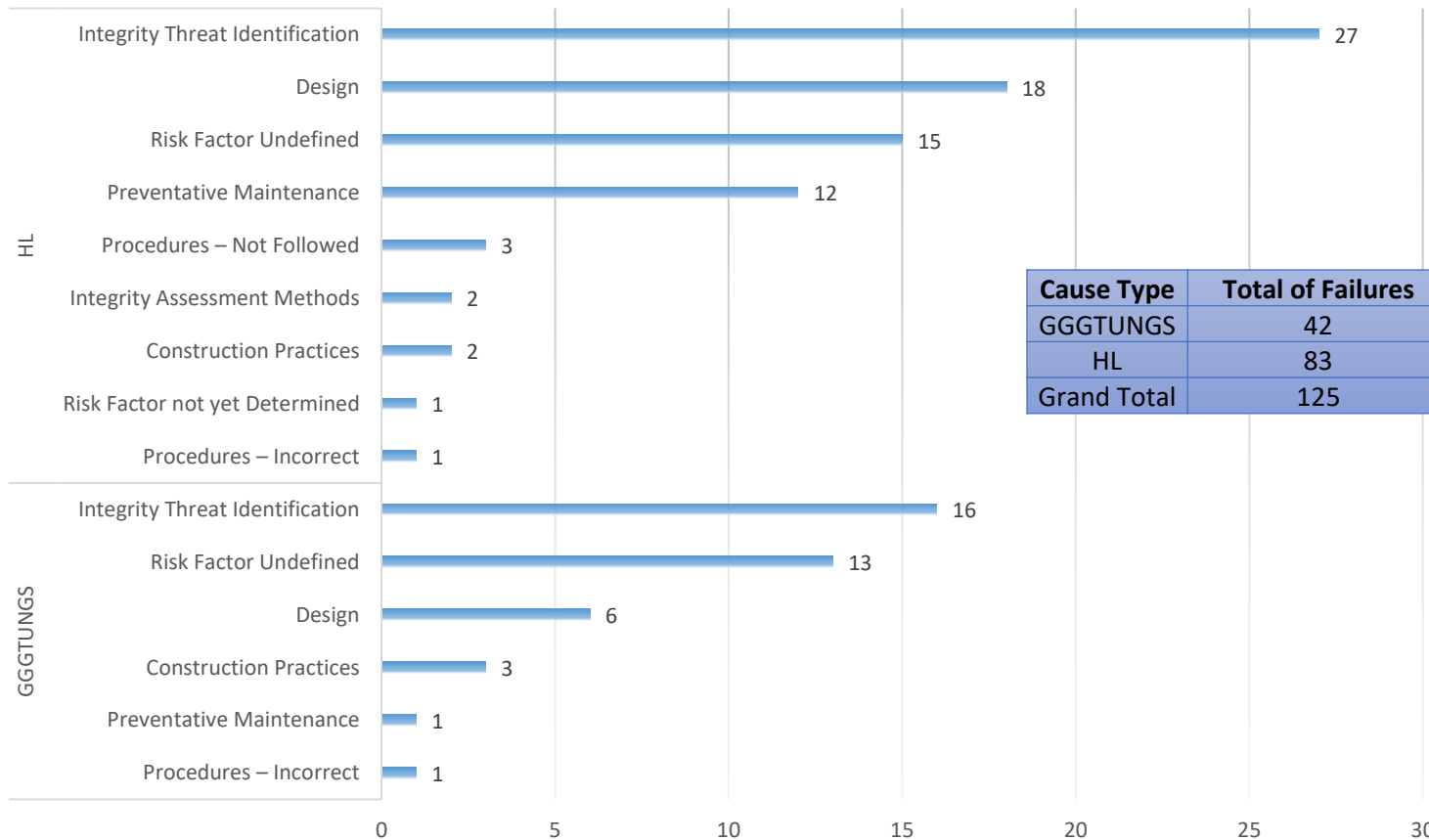
Cause Type	Total of Failures
GGGTUNGS	225
HL	748
Grand Total	973



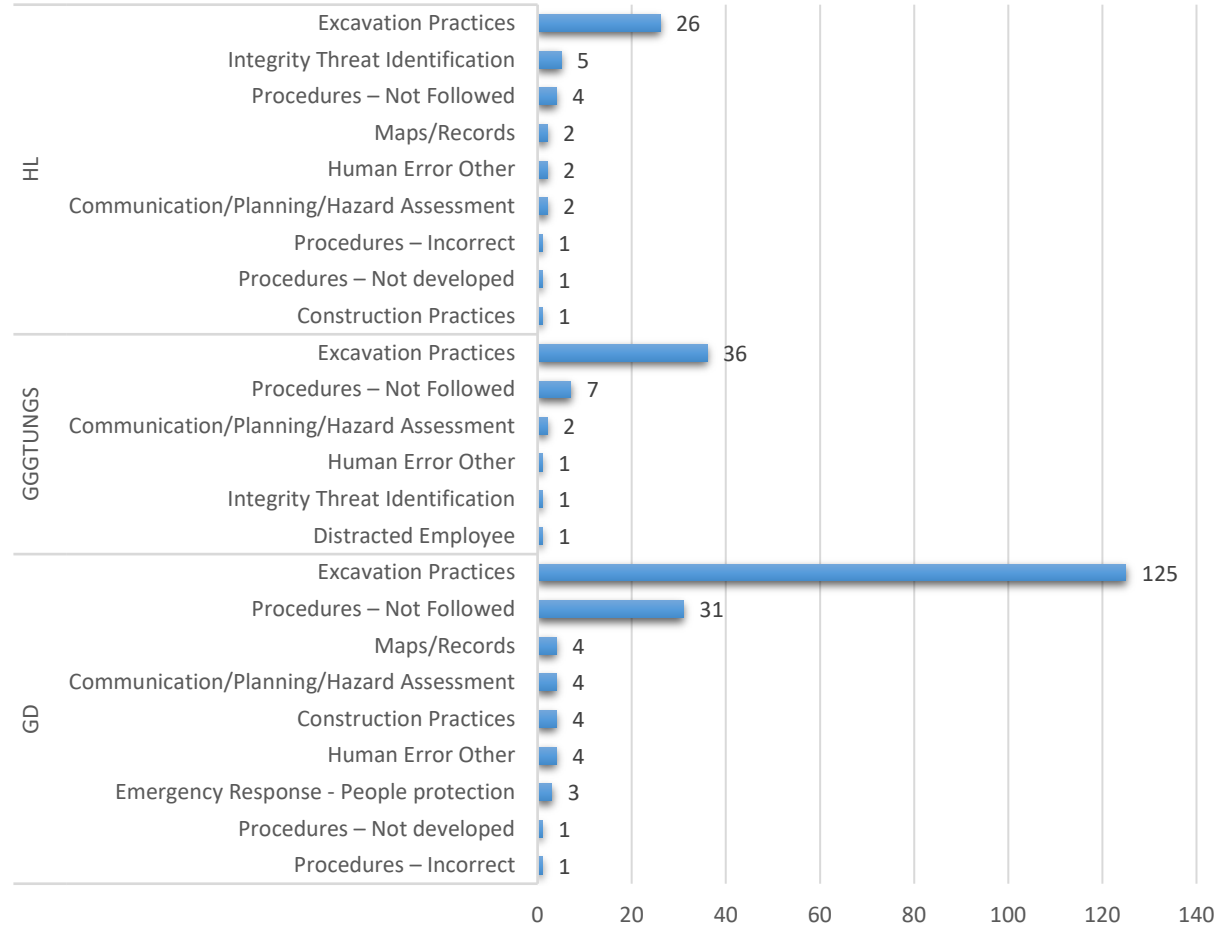
# Outside Force Damage – Risk Factors



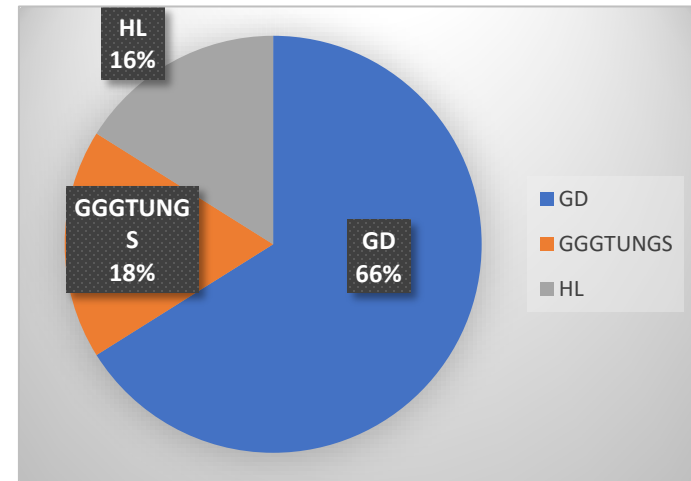
# Natural Force Damage – Risk Factors



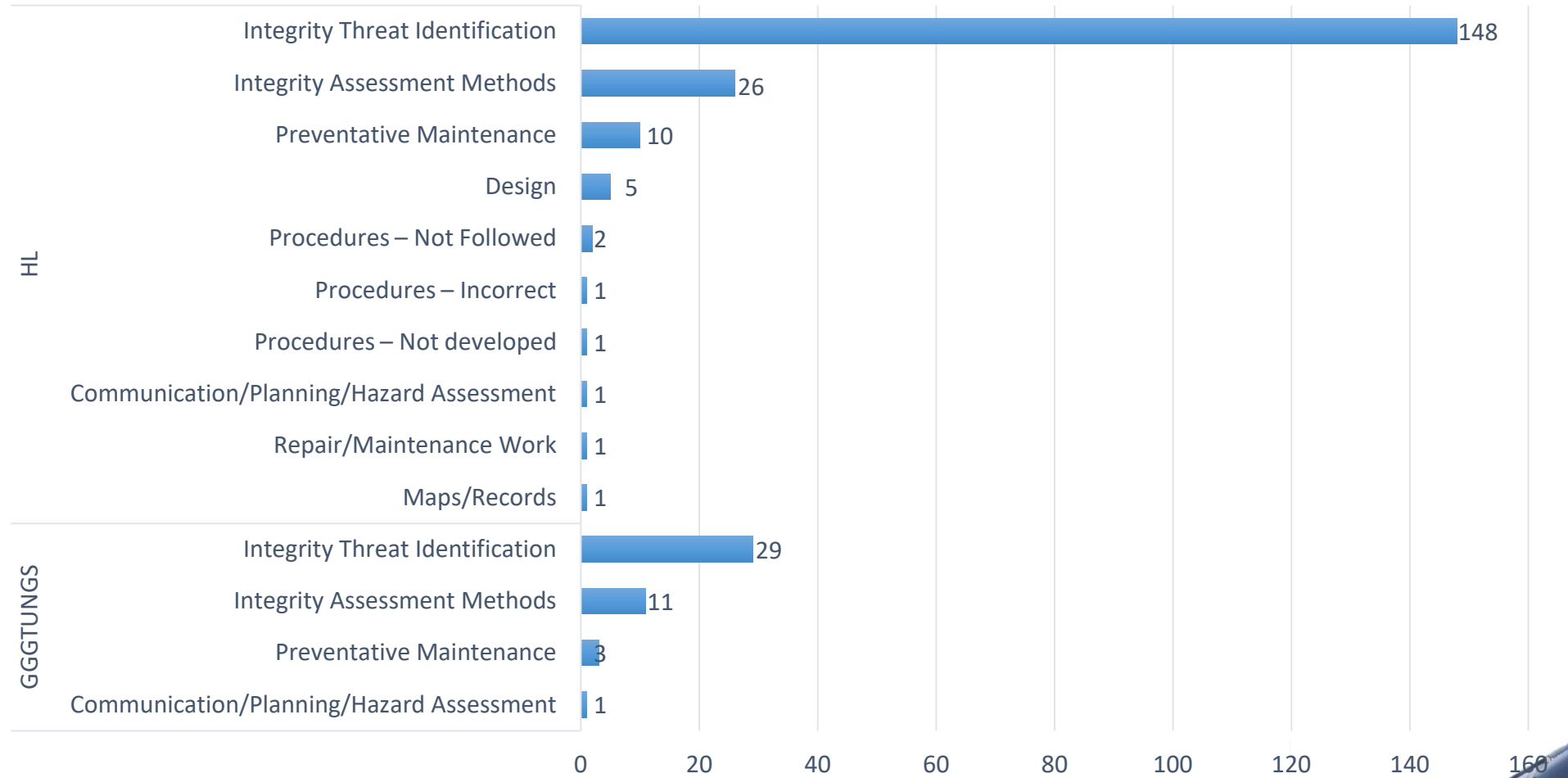
# Excavation Damage Risk Factors



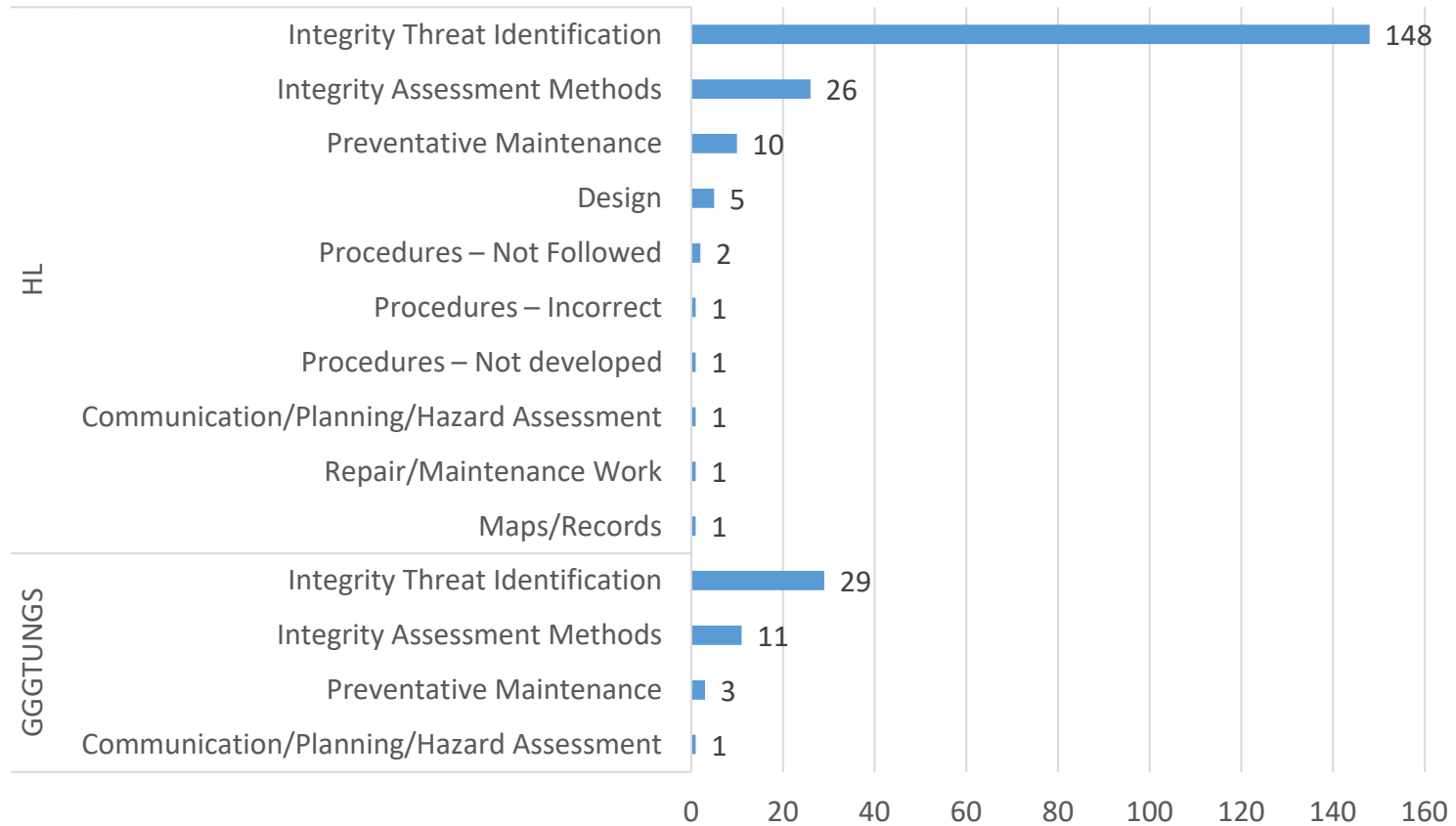
Cause Type	Total of Failures
GD	189
GGGTUNGS	51
HL	46
Grand Total	286



# Internal Corrosion

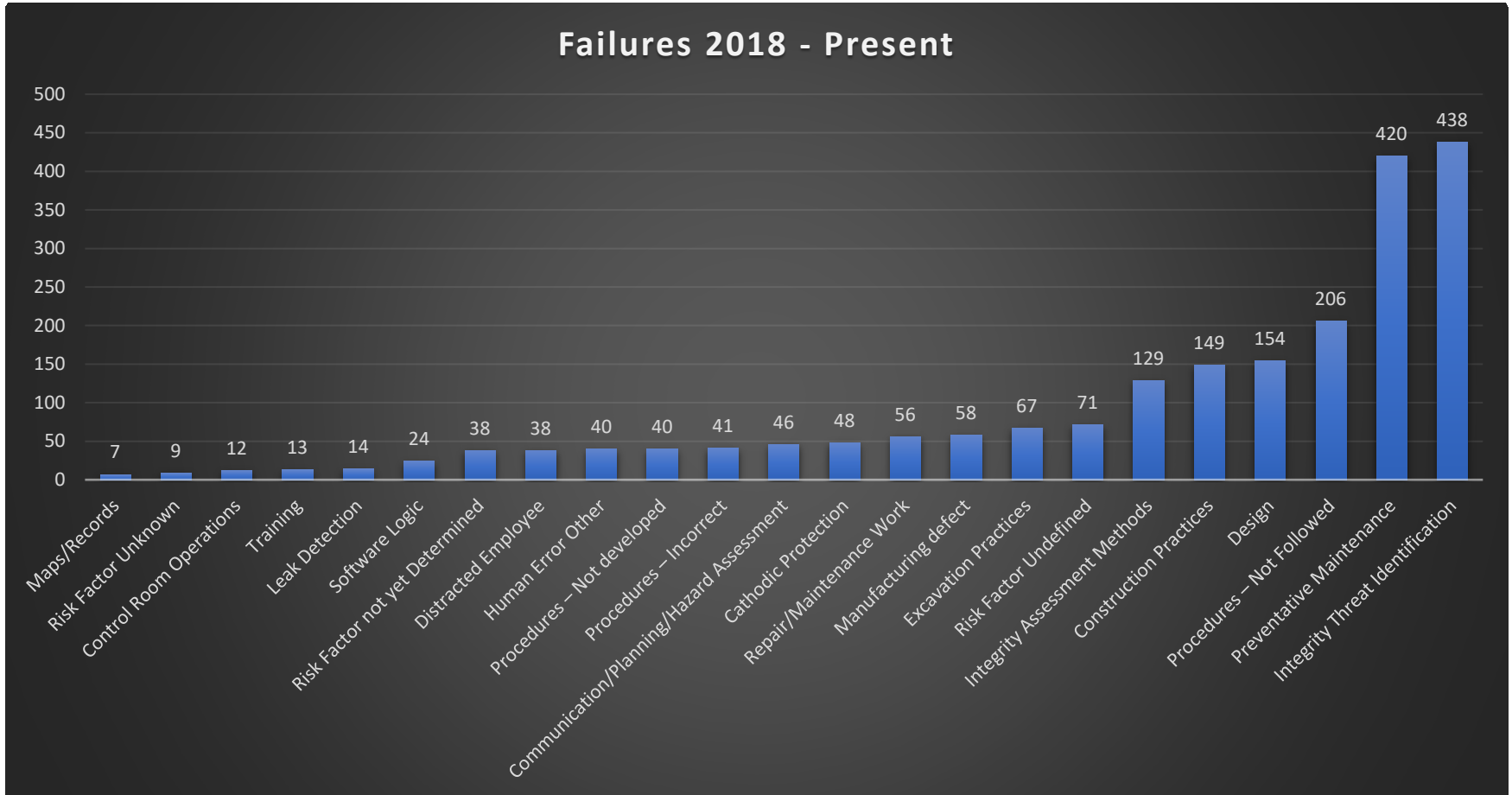


# External Corrosion





# All Risk Factors – All Products



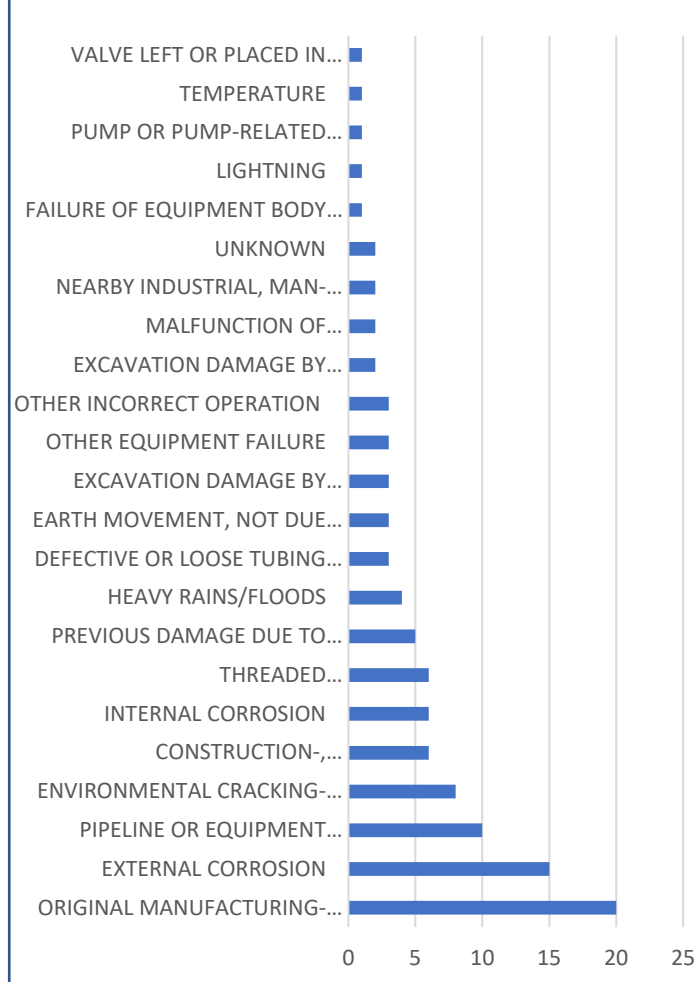
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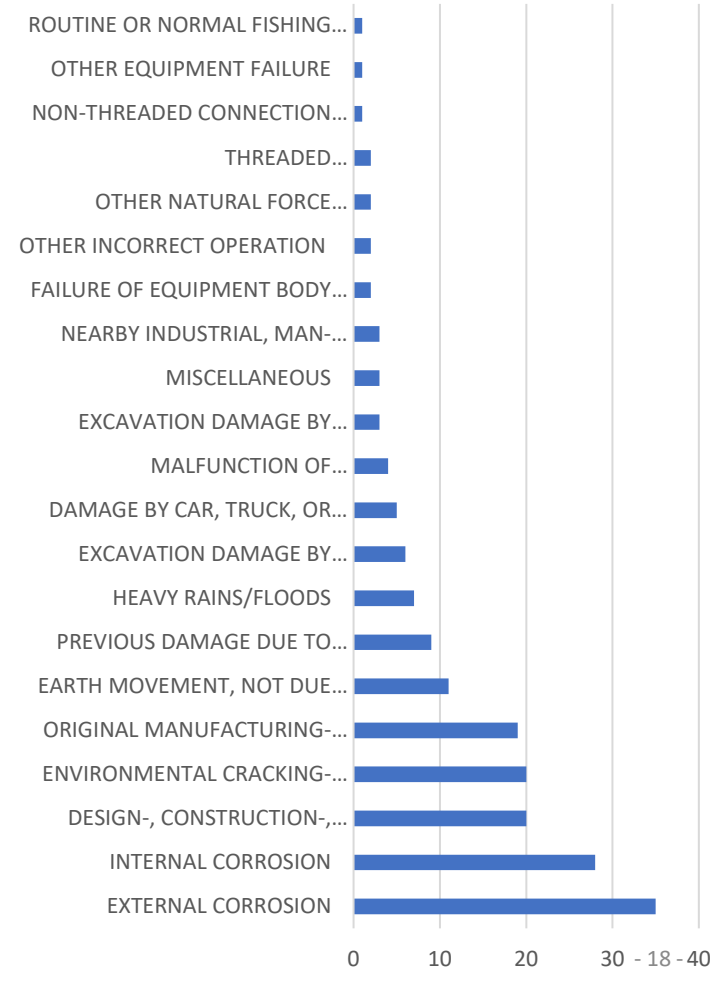


# Evaluation of Failures that resulted in Ruptures

## 108 Hazardous Liquids Ruptures

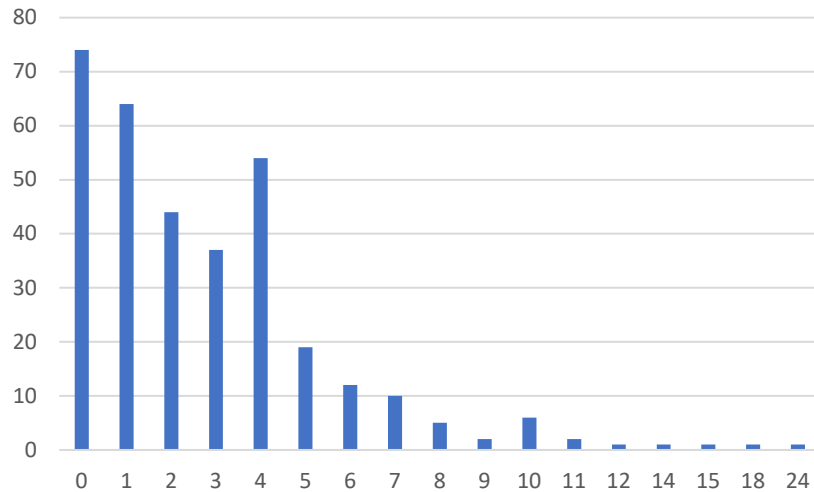


## 184 Gas Transmission Ruptures

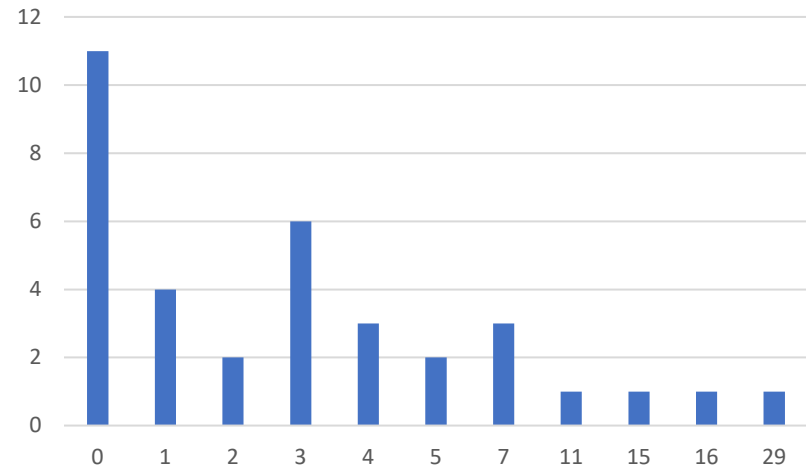


# External Corrosion After Tool Run

## HL Reportable External Corrosion Failures after 5yr Tool Run

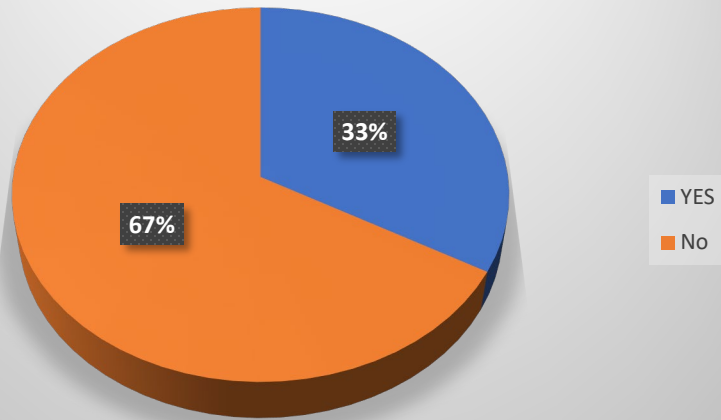


## GT Reportable External Corrosion Failures after 7yr Tool Run

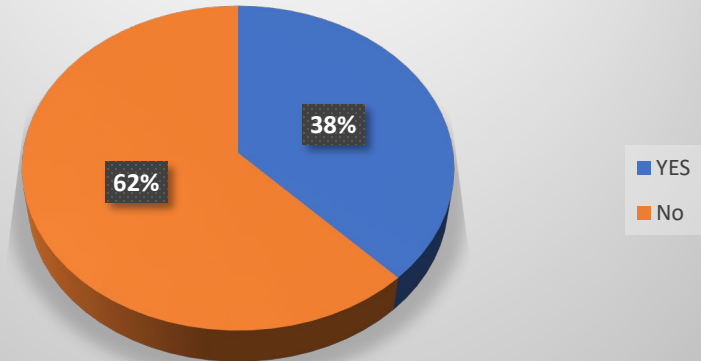


# Close Interval Survey

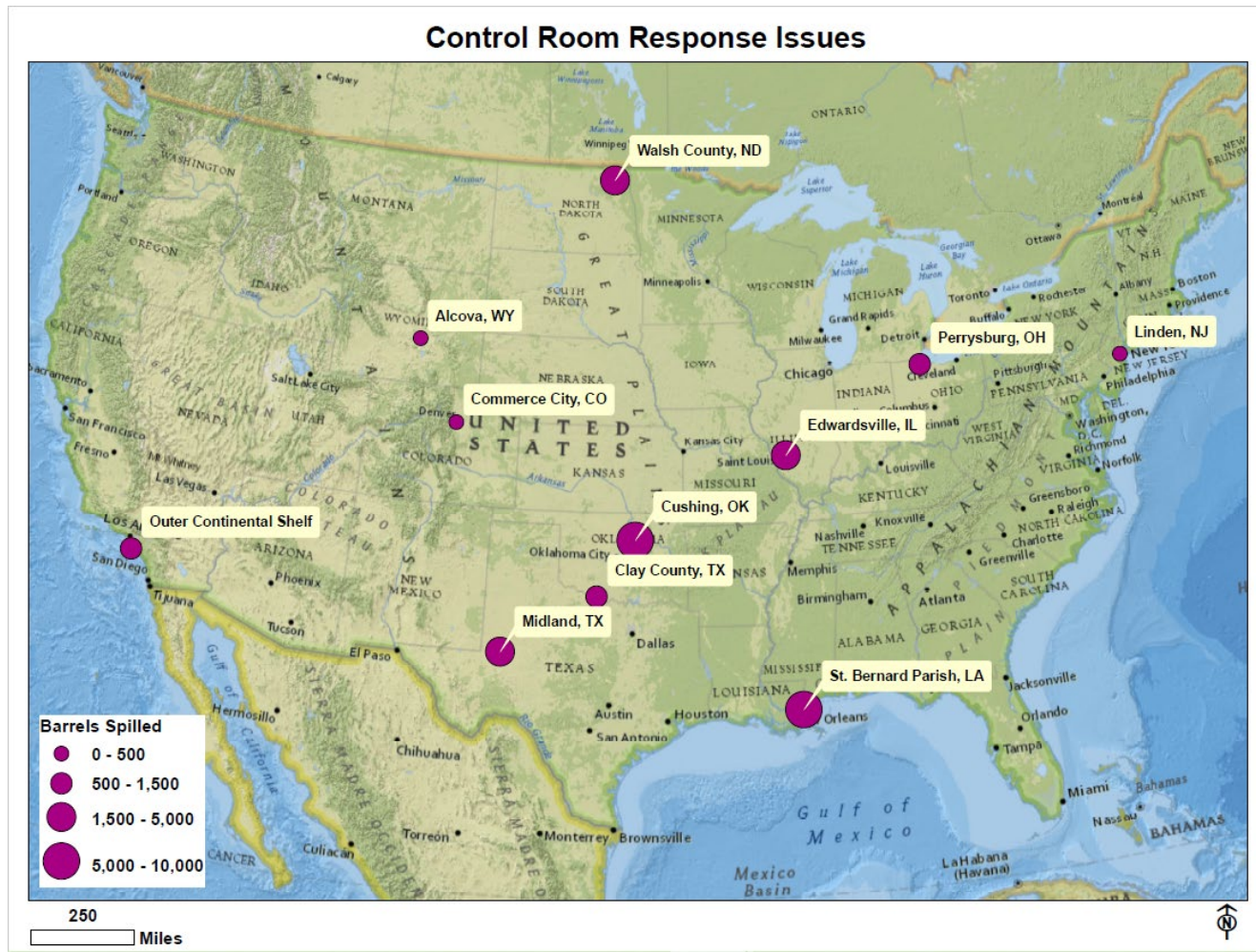
Was a CIS done on the HL pipeline with external corrosion failure?



Was a CIS done on the GT pipeline with external corrosion failure?



# Map of Recent Accidents were Control Room actions increase the consequence of the incident





# Recent Control Room Examples

- July 10, 2019 – Wichita Falls, Texas – 1100 Barrels of Crude
  - 12-Inch pipeline failure due to Selective Seam Weld Corrosion
  - Low suction pressure alarms – initially thought to be a power glitch
  - Booster pump was started and ran for 2 minutes and 16 seconds
- October 29, 2019 – Edinburg, North Dakota – 4515 Barrels of Crude
  - 30-Inch pipeline failure due to longitudinal seam weld fatigue crack
  - Pump station shut down on low suction pressure
  - Accompanied by discharge pressure drop and increased flow rate
  - Controller attempted restart but stopped after 5 seconds



# Recent Control Room Examples

- December 4, 2020 – Commerce City, Colorado – 487 Barrel Diesel Spill
  - 6-Inch pipeline failure due to Selective Seam Weld Corrosion and fatigue cracking
  - Flow and pressure alarms along with unintentional shutdown of downstream pump station
  - Controller shutdown the pipeline, but then re-started for 8 minutes before shutting down again
- March 16, 2021 – Linden, New Jersey – 353 Barrels of Unleaded Gasoline Released
  - 12-Inch pipeline rupture due to external corrosion
  - Uncommanded shutdown due to low suction pressure
  - High-High flow rate alarm and LDS Alarm
  - Controller suspected a control valve issue
  - Controller started booster pump but stopped after 30 seconds



# Recent Control Room Examples

- **October 1, 2021 – Long Beach, California – 588 Barrel Crude Oil Release**
  - 16-Inch pipeline rupture due to mechanical damage (anchor drag) sustained months earlier
  - Atmos LDS alarms were valid – Personnel thought issues were related to an operational upset
  - Multiple shutdowns and restarts were performed while attempting to troubleshoot
  
- **December 27, 2021 – Chalmette, Louisiana – 8325 Barrel Diesel Spill**
  - 16-Inch pipeline rupture due to external corrosion
  - Uncommanded shutdown due to low suction pressure, multiple alarms
  - Controller suspected a control valve issue
  - Operations and troubleshooting w/ multiple alarms and restarts continued most of the day
  - Pipeline was finally shutdown and rupture location was identified almost 3 hours later





# Recent Control Room Examples

- **March 11, 2022 - Edwardsville, Illinois – 3900 Barrel Crude Oil Release**
  - 22-Inch pipeline rupture at a girth weld due to creek-bed subsidence
  - Uncommanded Unit shutdown on low suction pressure
  - 2<sup>nd</sup> pump was started for a short time
  
- **April 12, 2022 – Perrysburg, Ohio – 1225 Barrel Gasoline Spill**
  - 10-Inch pipeline rupture due to external corrosion
  - Uncommanded shutdown – Unexplained pressure drop – Immediate spike in flow rate
  - Controller was concerned with LPG flashing at the end of the pipeline
  - Controller restarted the pipeline for 5 minutes before shutting down and isolating the pipeline



# Recent Control Room Examples

- May 15, 2022 – Midland, Texas – 4800 Barrels of Crude
  - 10-Inch pipeline rupture due to a fillet weld failure on a split tee – likely due to bending stress
  - Volume imbalance was detected, but operations continued for almost 7 hours
  - Controller eventually shutdown the pipeline based on SCADA data and LDS alarm
- June 19, 2022 – Alcova, Wyoming – 500 Barrels of Crude
  - Tubing failure on a pump unit for a 10-inch pipeline
  - Atmos LDS alarm was received on June 19– Controller thought it was a “false alarm”
  - Controller thought it was due to start-up of an intermediate pump
  - Pipeline was not shutdown until 8 hours later



# Recent Control Room Examples

- July 7, 2022 – Cushing, Oklahoma – 5768 Barrel Crude Oil Release
  - 20-Inch pipeline rupture due to a longitudinal seam defect
  - Pipeline was restarted after an uncommanded shutdown on low suction pressure



# High-Level Observations

- No apparent connection between
  - Operators
  - Procedures
  - Controllers
- Solution may include
  - Improve training and utilization of simulations
  - Better understanding of and response to abnormal operating conditions
  - One way or the other – get people to **THINK LEAK FIRST**



# In-Service Rupture of an ILI Reported Defect

- ILI Reported Anomaly
- Downgraded Using Dig History
- Inadequate Pressure Reduction
- Rupture Prior to Repair



# Natural Gas Transmission Rupture

- Rupture Defect Identified by ILI
- Not Actionable as Reported
- Corrosion Growth Rate Unknown
- Anomaly Interaction was Non-Conservative



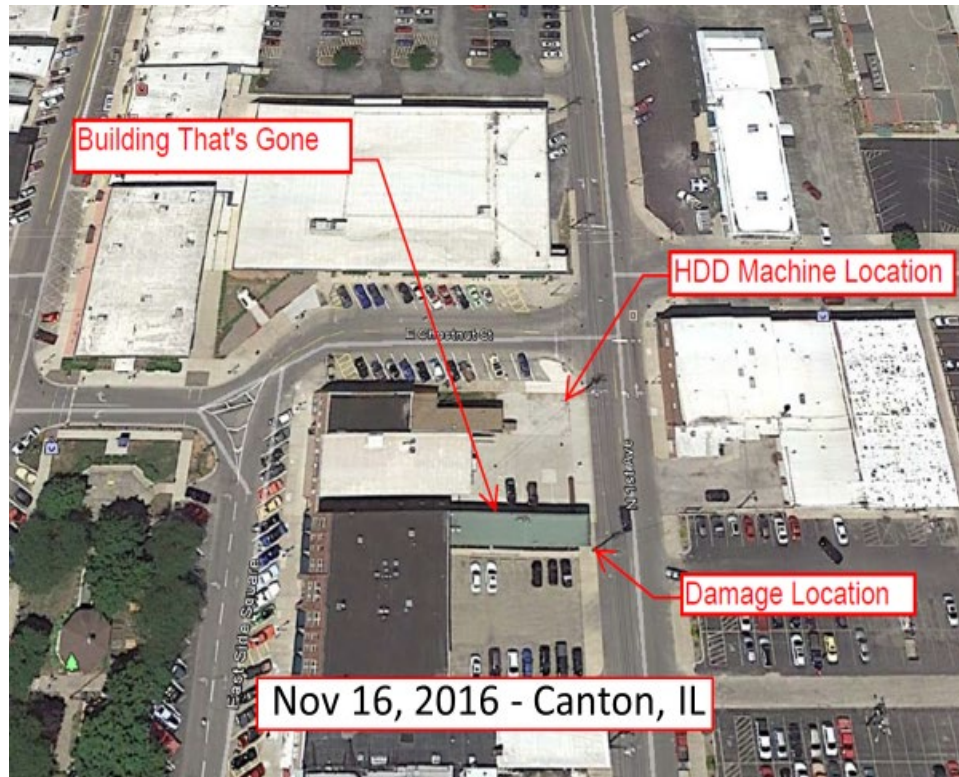
# Why Are We Missing These?

- Anomaly Interaction Criteria
  - Treated as Individual Defects When They Actually Combine
  - We Can Prevent Failures by Adding Conservatism
- Frequency
  - Are we Seeing a “Just in Time” Mentality?
  - Maybe Frequency Should Depend on What we Know/Don’t Know
- Outliers
  - What Affects ILI Accuracy?
- Overconfidence
  - Tool Accuracy
  - Failure Pressure Calculations





# Excavation Damage Due to HDD





# A Small Service Line!



- Damage to a 1-inch PE service line
- 911 Not Contacted Immediately
- Gas Company was On-site
- 1 Fatality - 12 Injuries
- Approximately 2-Hours until Explosion



# Excavation Damage Due to HDD

April 10, 2019 – Durham, NC





# THERE'S A LOT OF THIS GOING ON!

- Cable installation using HDD
- Damaged 2-inch main
- 2 Fatalities, 5 Reportable Injuries
- Over \$20 million in damages
- Approximately one hour from damage to ignition



# Trenchless Technology

- Unique characteristics of HDD increase the potential consequences of damage
  - Typically, congested areas/pavement
  - Gas migration vs. direct to atmosphere
  - Release isolation complexity increases
  - Are emergency procedures adequate? Isolation Plan?



# Considerations

- Require visual verification (Daylighting) of crossings
- Evaluate one-calls for HDD – Know Where They're Crossing You – Know Who's Doing the Work – Know They Excavate Safely
- Pre-Plan Emergency Response for Each Known Crossing
- Treat Every Single Crossing Knowing Lives Are in the Balance
- Train Personnel on the Special Concerns with HDD



# Emergency Response – Lessons Learned

- Many High Consequence Failures Show Ineffective Emergency Response
- The Cause of the Release isn't always the Story – 80,000 vs 50
- Does the Inherent Safety of Gas result in Complacency? Bad Practices? Overconfidence?
- Are Your Procedures Clearly - Written?? Understood?? Followed??
- **TWO BIG THINGS** - Use your CGIs – Isolate a Safe Distance From the Release

